

› OPM'S LATEST DEVELOPMENTS BY TNO

C. G. Machado, P. J. P. Egberts, E. G. D. Barros, H. Slot

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TNO innovation
for life

SUMMARY

- › On-going developments within TNO
 - › Outputs (PRT report, summary curves, well potential, etc)
 - › Salt precipitation module
 - › Radial grid
 - › Applications/Testing

TNO PROJECTS CURRENTLY USING OPM-FLOW

- › OPM software development
- › Salt Precipitation Modeling
- › Geothermal Energy Optimization
- › EVEReST (Field Development Optimization), and History matching (ERT)
- › Storage integrity tool (CO₂ / H₂ Injection)
- › Earthquakes Impact Mitigation (as the flow module coupled with MACRIS)
- › RoSim (alternative to TNO 's in-house DoubletCalc2D/3D)
- › Etc...

SALT PRECIPITATION PROBLEM

- › Salt precipitation in gas reservoirs can be a huge issue for operators
 - › Clogging results in severe production decline

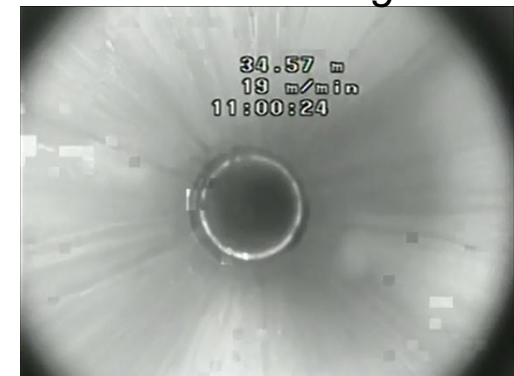
- › ~50 of 330 Dutch gas fields suffer from salt precipitation
 - › this number is increasing in time

- › Precipitation occurs near the wellbore
 - › Accumulation in well bore
 - › Soaking with small amounts of fresh water restores production

Before washing



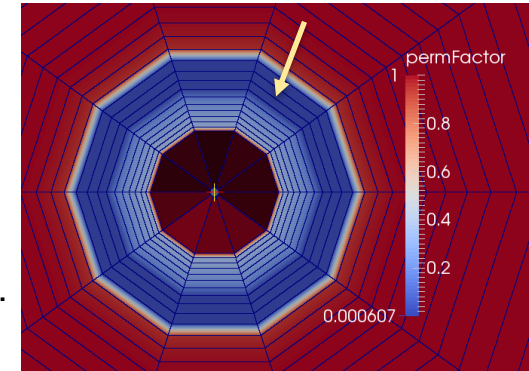
After washing



SALT PROJECTS

- › 2013-2016
 - › Near well bore modelling using **Dumu^x** by Universität Stuttgart
 - › Added specific salt related physics:
 - › Vapour pressure lowering, Capillary pressure correction, ...
- › October 2019 (Current JIP Project)
 - › Optimization of production
 - › Washing strategies (when, how much, for how long)
 - › Incorporation of salt precipitation in OPM flow motivated by
 - › Performance increasement
 - › Usability; larger potential user group
 - › Presence of well models. Three-phase flow (gas condensate reservoirs)

Permeability reduced to zero



APPROACH (HIGH-LEVEL)

- › Step 1: Incorporate Salt component
 - › Salt transport equation + precipitation
 - › Primary variable switching
 - › Salt concentration depending fluid properties (viscosity, density)
 - › Validation using ECLIPSE/Dumux
 - › Changing permeability $k = k(\phi)$

- › Step 2: Incorporate water evaporation into gas
 - › Modify black-oil equation
 - › Relation for vaporized water in gas (pressure and salt dependent)
 - › Validate water-gas system with Dumux implementation

Step 1: Adds on
black-oil equations

Step 2: Changes
black-oil equations

SALT TRANSPORT EQUATION

› Transport equation:
$$\frac{\partial \phi_0 m_\phi (b_w s_w C_w^{NaCl} + s_s \rho^{NaCl})}{\partial t} + \nabla \cdot (C_w^{NaCl} b_w v_w) + C_w^{NaCl} q_w = 0$$

- C_w^{NaCl} : Salt concentration in water [kg/Sm³].
- s_s : (volume) saturation of deposited salt, assumed to be immobile.
- $C_w^{NaCl} q_w$: Source/sink term for wells [kg/s].
- ρ^{NaCl} : Density of solid salt [kg/m³]

› Similar equation (but without precipitation) in Eclipse and OPM (very recent, by Trine S. Mykkeltvedt)

› The closure relation for saturations becomes:
$$s_w + s_o + s_g + s_s = 1$$

› Primary variable switching:

› $C_w^{NaCl} > C_{w,sol}^{NaCl} \rightarrow$ primary variable becomes s_s

› $s_s < 0 \rightarrow$ primary variable becomes C_w^{NaCl}

$C_{w,sol}^{NaCl}$: solubility limit

› Remark: Formulation differs from Dumux that use sources and sinks for dissolution/precipitation

BLACK-OIL FORMULATION, WITH WATER VAPORIZATION

$$\text{Oil:} \quad \frac{\partial}{\partial t} [\varphi_o m_\varphi (b_o s_o + r_{og} b_g s_g)] + \nabla \cdot (b_o v_o + r_{og} b_g v_g) + q_o = 0$$

$$\text{Gas:} \quad \frac{\partial}{\partial t} [\varphi_o m_\varphi (b_g s_g + r_{go} b_o s_o)] + \nabla \cdot (b_g u_g + r_{go} b_o v_o) + q_g = 0$$

$$\text{Water:} \quad \frac{\partial}{\partial t} [\varphi_o m_\varphi (b_w s_w + r_{wg} b_g s_g)] + \nabla \cdot (b_w v_w + r_{wg} b_g u_g) + q_w = 0$$

with r_{wg} : vaporized water in the gas phase

v_α : the velocities of phase α (= gas, oil or water).

$b_\alpha = 1/B_\alpha$ with B_α the formation volume factor of phase α (ratio of reservoir to standard condition volumes [Rm³/Sm³])

s_α : the saturation of phase α

r_{og} : vaporized oil in the gas phase (ratio of volumes at standard condition Vo/Vg [Sm³/Sm³] from a volume of gas at reservoir conditions)

r_{go} : solution of gas in oil phase (ratio of volumes at standard Vg/Vo [Sm³/Sm³] from a volume of oil at reservoir conditions)

q_α : source /sink terms for phase α , typically associated to production/injection wells

m_φ : porosity multiplication factor

T : temperature, which we will assume fixed

p_g : pressure in gas phase

PRIMARY VARIABLES

For three-phase case and a grid with n cells, the material balances give us $4n$ equations.
We can define as primary variables:

Phases present

water, gas and oil

gas and oil

water and gas

water and oil

water, gas, oil, salt

gas and oil, salt

water and gas, salt

water and oil, salt

Primary variables

$C_w^{NaCl}, p_o, s_g, s_w$

s_s, p_o, s_g, r_{wg}

$C_w^{NaCl}, p_g, s_g, r_{og}$

$C_w^{NaCl}, p_o, s_w, r_{go}$

s_s, p_o, s_g, s_w

s_s, p_o, s_g, r_{wg}

s_s, p_g, s_g, r_{og}

s_s, p_o, s_w, r_{go}

Possible convergence issues?

INPUT FILE

› Keywords:

› RUNSPEC:

- › **VAPWAT**: Activate water vaporization, PROPS should have a RWG table.
- › **BRINE**: Activate salt transport equation (we assume NaCl only)
- › **PRECSALT**: Activate Salt Precipitation. PROPS should have SALTSOL

› PROPS

- › **SALTSOL**: Solubility limits
- › **PERMRED**: Defines the permeability multiplier as function of porosity for a reference k
- › **PVTWSALT**: Defines PVT data for brine
- › **PVTGW, PVTGWO**: Gas PVT properties with RWG column
- › **RWGSALT**: Define water vaporization vs. pressure and salt conc.

**New
Exists**

› SOLUTION:

- › **SALTVD, SALTPVD**: Initial salt concentrations in water and **rock**

› SCHEDULE:

- › **WSALT**: Defines the salt concentration in water injectors

PVT TABLES

--
 -- GAS PVT TABLE FOR WET GAS

--
 PVTG

PSIA	RV STB/MSCF	BG RB/MSCF	VISC CPOISE
300	0.000132	0.042340	0.01344
	0	0.042310	0.01389 /
600	0.000124	0.020460	0.01420
	0	0.020430	0.01450 /
900	0.000126	0.013280	0.01526
	0	0.013250	0.01532 /
1200	0.000135	0.009770	0.01660
	0	0.009730	0.01634 /
1500	0.000149	0.007730	0.01818
	0	0.007690	0.01752 /
1800	0.000163	0.006426	0.01994
	0	0.006405	0.01883 /
2100	0.000191	0.005541	0.02181
	0	0.005553	0.02021 /
2400	0.000225	0.004919	0.02370
	0	0.004952	0.02163 /

/ TABLE NO. 1

--
 -- GAS PVT TABLE FOR WET GAS

--
 PVTGW

PSIA	RWG STB/MSCF	BG RB/MSCF	VISC CPOISE
300	0.000132	0.042340	0.01344
	0	0.042310	0.01389 /
600	0.000124	0.020460	0.01420
	0	0.020430	0.01450 /
900	0.000126	0.013280	0.01526
	0	0.013250	0.01532 /
1200	0.000135	0.009770	0.01660
	0	0.009730	0.01634 /
1500	0.000149	0.007730	0.01818
	0	0.007690	0.01752 /
1800	0.000163	0.006426	0.01994
	0	0.006405	0.01883 /
2100	0.000191	0.005541	0.02181
	0	0.005553	0.02021 /
2400	0.000225	0.004919	0.02370
	0	0.004952	0.02163 /

/ TABLE NO. 1

PVT TABLES

```
--
-- WATER EVAPORATION TABLE FOR BRINE
--
```

RWGSALT

```
-- PRES      SALTCON      RWG
-- PSIA      LB/STB      STB/MSCF
```

```
-----
PRES1      SAL11      RWG11
           SAL21      RWG 21
           ...
           SALN1      RWGN1/
PRES2      SAL12      RWG12
           SAL22      RWG22
           ...
           SALN2      RWGN2 /
           ...
PRESM      SAL1M      RWG1M
           SAL2M      RWG2M
           ...
           SALNM      RWGNM /
```

```
--
-- GAS PVT TABLE FOR WET GAS
--
```

PVTGWO

```
-- PRES      RWG      RV      BG      VISC
-- PSIA      STB/MSCF  STB/MSCF  RB/MSCF  CPOISE
```

```
-----
300      0.000132  0.000132  0.042340  0.01344
           0      0      0.042310  0.01389 /
600      0.000124  0.000124  0.020460  0.01420
           0      0      0.020430  0.01450 /
900      0.000126  0.000126  0.013280  0.01526
           0      0      0.013250  0.01532 /
1200     0.000135  0.000135  0.009770  0.01660
           0      0      0.009730  0.01634 /
1500     0.000149  0.000149  0.007730  0.01818
           0      0      0.007690  0.01752 /
1800     0.000163  0.000163  0.006426  0.01994
           0      0      0.006405  0.01883 /
2100     0.000191  0.000191  0.005541  0.02181
           0      0      0.005553  0.02021 /
2400     0.000225  0.000225  0.004919  0.02370
           0      0      0.004952  0.02163 /
```

/ TABLE NO. 1

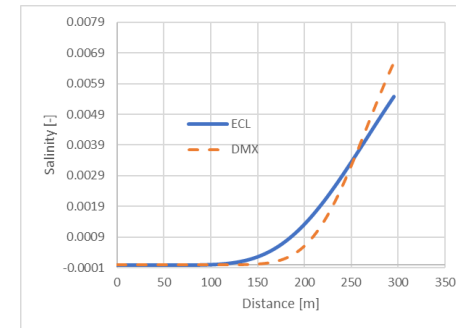
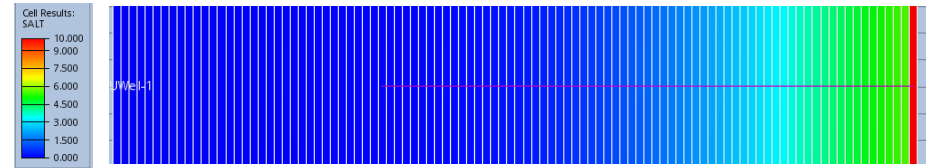
BENCHMARK (DUMU^x)

- › Issues to set up an OPM case
 - › Two-phase specifying gas-water capillary pressure seems not possible
 - › Table SGWFN not working
 - › PVTWSALT interpolation

- › For now brine tracking compared with ECLIPSE
 - › Comparison not good (yet)
 - › Difference in PVT properties (Cw)

```

--
-- GAS-WATER RELATIVE PERMEABILITY TABLES (SGWFN)
SGWFN
-- SG KRG KRW PCGW
-- FRAC      PSIA
-----
    
```



PERMEABILITY REDUCTION

$$k = m_k(\varphi)k_0$$

- › Porosity change is directly related to the change of the (volume) saturation s_s :

$$\varphi = (1 - s_s)\varphi_0$$

- › The associated permeability reduction will be calculated using a correlation such as:

Kozeny-Carman (extended)

$$k/k_0 = \left(\frac{\varphi - \varphi_c}{\varphi_0 - \varphi_c}\right)^a \left(\frac{1 - \varphi_0 + \varphi_c}{1 - \varphi + \varphi_c}\right)^b$$

Verma-Pruess

$$\frac{k}{k_0} = \max\left(\frac{1}{(1 - \varphi_r)^2} \left(\frac{\varphi}{\varphi_0} - \varphi_r\right)^2, 0\right)$$

Power law

$$\frac{k}{k_0} = \left(\frac{\varphi}{\varphi_0}\right)^\gamma$$

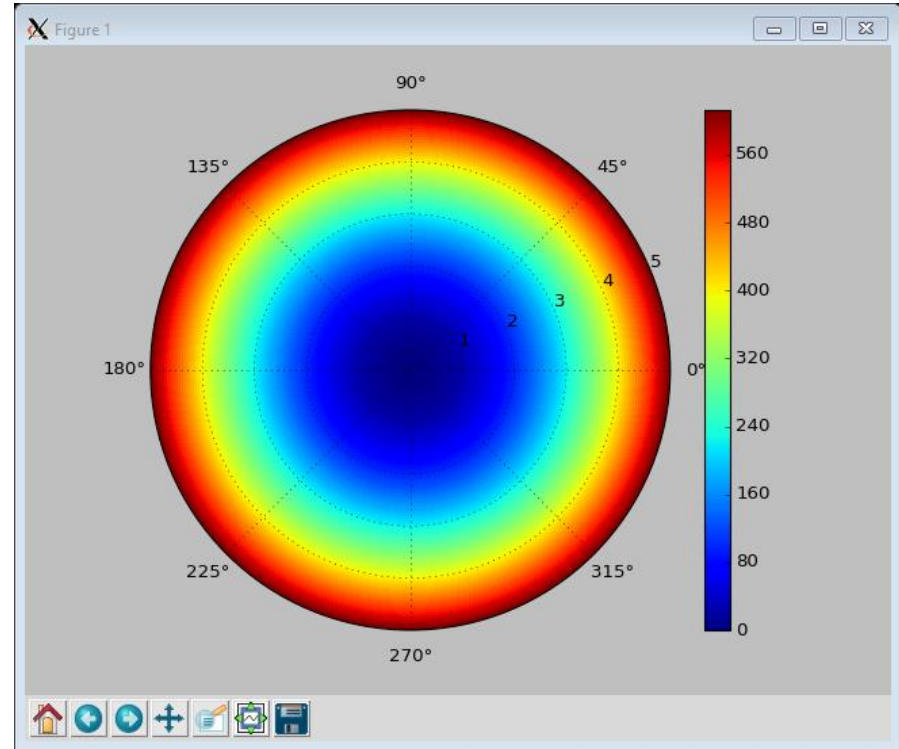
```

--
-- PERMEABILITY REDUCTION TABLE FOR SALT PRECIPITATION
-- FOR A POROSITY OF REFERENCE
--
PERMRD
-- PHI          M
-- -----
0          0
PHI1      M1
...
PHIREF    1
...
PHIMAX    MMAX
    
```

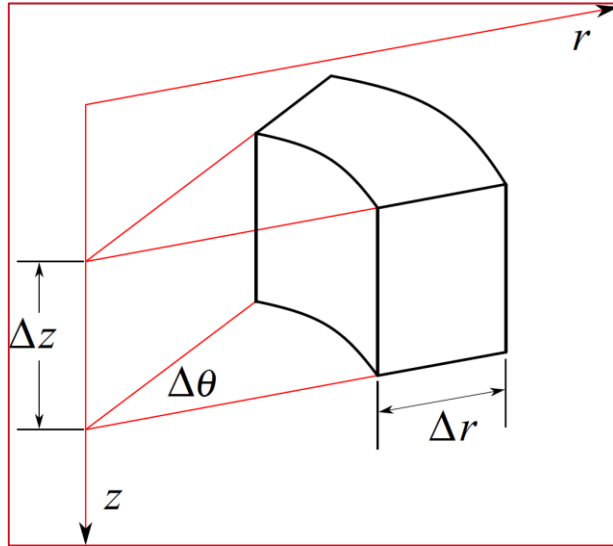
RADIAL GRID

- › Motivation:
 - › Capture near wellbore effects
 - › Local grid refinement

- › Keywords:
 - › RADIAL
 - › COORDSYS
 - › COMP/INCOMP
 - › INRAD
 - › DRV
 - › DTHETAV
 - › PERMR
 - › PERMTHT



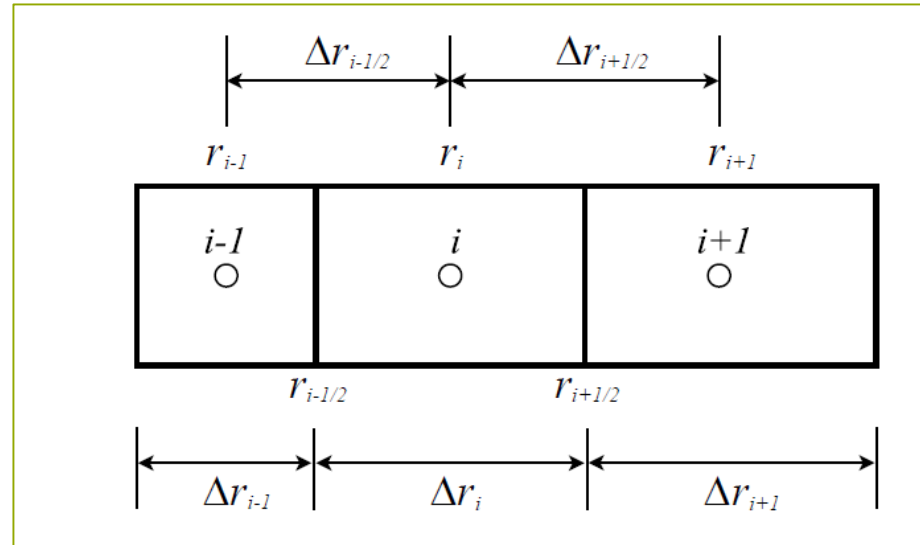
RADIAL DISCRETIZATION



Gridblock volume

$$V_{b_{i,j,k}} = \frac{(r_{i+\frac{1}{2},j,k}^2 - r_{i-\frac{1}{2},j,k}^2) \Delta\theta_{i,j,k} \Delta z_{i,j,k}}{2}$$

Logarithmic Spacing



$$r_{i+\frac{1}{2},j,k} = \frac{r_{i+1,j,k} - r_{i,j,k}}{\ln\left(\frac{r_{i+1,j,k}}{r_{i,j,k}}\right)}, \quad r_{i-\frac{1}{2},j,k} = \frac{r_{i,j,k} - r_{i-1,j,k}}{\ln\left(\frac{r_{i,j,k}}{r_{i-1,j,k}}\right)}$$

RADIAL TRANSMISSIBILITIES

$$R_{\alpha,i} = \frac{\phi_{ref,i} V_i}{\Delta t} (A_{\alpha,i} - A_{\alpha,i}^0) + \sum_{j \in C(i)} u_{\alpha,ij} + q_{\alpha,i} = 0$$



$$T_{r_{i \pm \frac{1}{2}, j, k}} = \frac{r_{i \pm \frac{1}{2}, j, k} k_{r_{i \pm \frac{1}{2}, j, k}} \Delta \theta_{i, j, k} \Delta z_{i, j, k}}{\Delta r_{i \pm \frac{1}{2}, j, k}} \left(k_r \frac{b}{\mu} \right)_{i \pm \frac{1}{2}, j, k}$$

$$T_{\theta_{i, j \pm \frac{1}{2}, k}} = \frac{k_{\theta_{i, j \pm \frac{1}{2}, k}} \ln \left(\frac{r_{i + \frac{1}{2}, j, k}}{r_{i - \frac{1}{2}, j, k}} \right) \Delta z_{i, j, k}}{\Delta \theta_{i, j \pm \frac{1}{2}, k}} \left(k_r \frac{b}{\mu} \right)_{i, j \pm \frac{1}{2}, k}$$

$$T_{z_{i, j, k \pm \frac{1}{2}}} = \frac{(r_{i + \frac{1}{2}, j, k}^2 - r_{i - \frac{1}{2}, j, k}^2) k_{z_{i, j, k \pm \frac{1}{2}}} \Delta \theta_{i, j, k}}{2 \Delta z_{i, j, k \pm \frac{1}{2}}} \left(k_r \frac{b}{\mu} \right)_{i, j, k \pm \frac{1}{2}}$$

PERMEABILITIES IN RADIAL DIRECTION

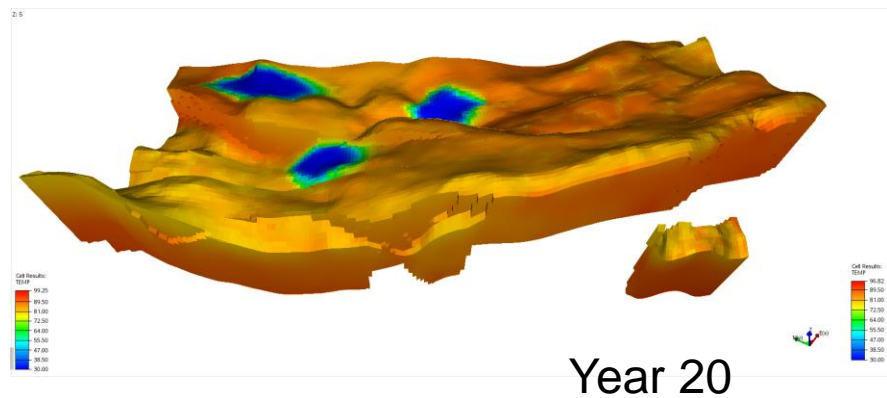
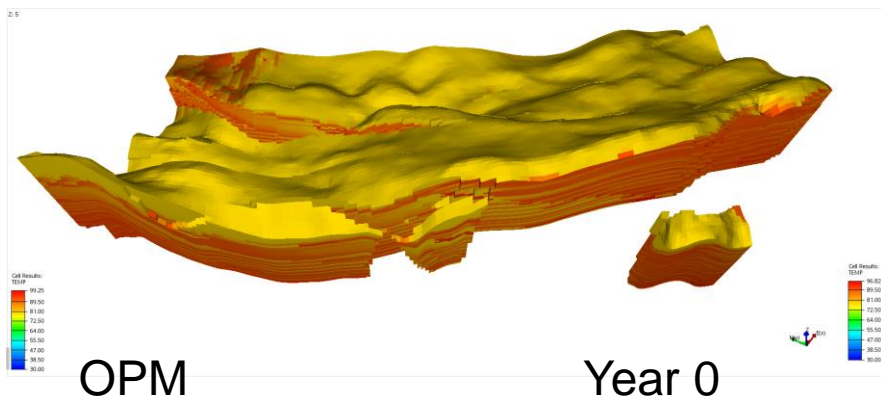
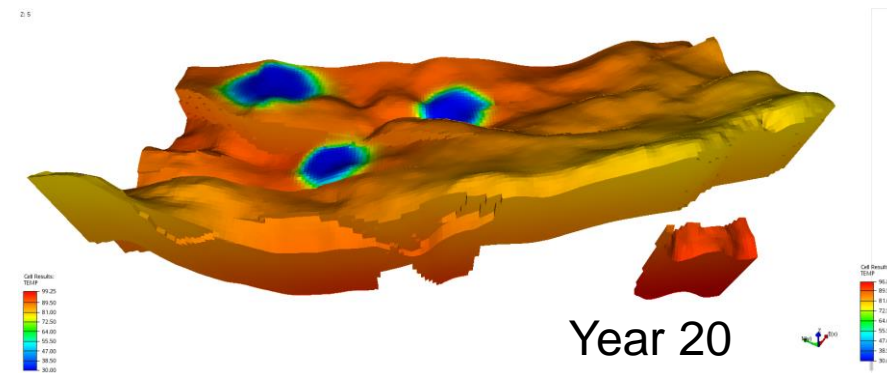
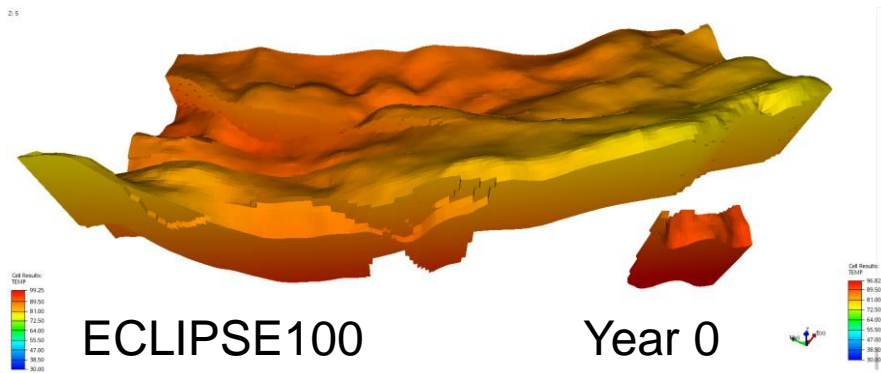
$$k_{r_{i+\frac{1}{2},j,k}} = \frac{k_{i,j,k} k_{i+1,j,k} \ln \left(\frac{r_{i+1,j,k}}{r_{i,j,k}} \right)}{k_{i,j,k} \ln \left(\frac{r_{i+1,j,k}}{r_{i+\frac{1}{2},j,k}} \right) + k_{i+1,j,k} \ln \left(\frac{r_{i+\frac{1}{2},j,k}}{r_{i,j,k}} \right)}$$

$$k_{r_{i-\frac{1}{2},j,k}} = \frac{k_{i-1,j,k} k_{i,j,k} \ln \left(\frac{r_{i,j,k}}{r_{i-1,j,k}} \right)}{k_{i-1,j,k} \ln \left(\frac{r_{i,j,k}}{r_{i-\frac{1}{2},j,k}} \right) + k_{i,j,k} \ln \left(\frac{r_{i-\frac{1}{2},j,k}}{r_{i-1,j,k}} \right)}$$

GEOTHERMAL ENERGY

- › Needed in short term
 - › Working viscosity and density dependency in temperature (fix convergence issues)
 - › Well temperature output
- › Long term
 - › DUALPORO/DUALPERM (Eclipse)
 - › MINC (popular in Geothermal, TOUGH2)

OPM TEMPERATURE INITIALIZATION



PERFORMANCE OF A SINGLE RUN

› OPM Flow 23.10.2019; 30 years run

Model and active cells	ECLIPSE		OPM	OPM with amg and tuning	
	NO VISC	VISC		NO VISC	VISC
NO_TEMP 500 000	1m 40s		7h 30m	26min	
TEMP 400 000	x	7m 45s	x	1h 30m	8h
TEMP 500 000	2m 50s	7m 40s	x	7h	14h
TEMP 1 000 000	x	14m 15s	x	12h	70h

WELLBORE PRODUCED HEAT

To calculate the heat produced (H) over all n well connections:

$$H = \sum_{j=1}^{j=n} q_{w,j} \times \rho_j \times T_j \times C_w \times \Delta t$$

$q_{w,j}$ flow rate per connection [m³/d]

C_w Heat capacity [kJ/kg/K]

ρ density [kg/m³]

T temperature [K]

Δt time period [d]

(All units in METRIC)

The average temperature \bar{T} can then be calculated as:

$$\bar{T} = \frac{H}{Q \times \rho \times C_w \times \Delta t}$$

If we assume that heat capacity and density are constant, this reverts to the connection flow averaged temperature.

A nighttime photograph of a city street. In the foreground, a modern, curved pedestrian bridge with a metal mesh railing is illuminated from below. The background shows a multi-story brick building on the left and a modern glass-walled building on the right. Long, horizontal light trails in green and white are visible across the scene, suggesting motion. The sky is dark, and the overall atmosphere is urban and contemporary.

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ATTENTION**

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