

OPM Flow – overview and demonstration

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SINTEF Digital, Mathematics and Cybernetics

MSO4SC workshop
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Overview of talk

Reservoir simulation

Mathematical formulation

Implementation with automatic differentiation

What next?

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What is reservoir simulation

Simulation of *porous medium* flow in *subsurface* reservoirs.

Examples of use:

- ▶ Energy industry
 - ▶ Forecasting and optimizing oil and gas production.
 - ▶ Forecasting and optimizing geothermal energy production.
- ▶ Environmental management
 - ▶ Groundwater flows and pollutants
 - ▶ CO₂ storage

Reservoir simulators solve *systems of nonlinear PDEs* that are coupled to *well/facility models*.

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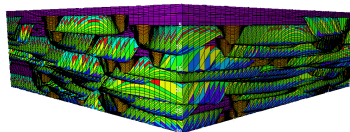
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- ▶ The models are highly nonlinear.

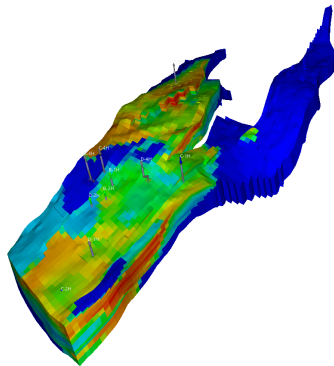
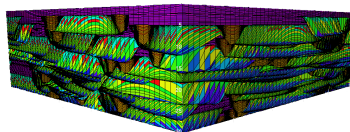
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Why does it require HPC/Cloud

- ▶ Model sizes increasing (Saudi-Aramco record: 1e12 cells)
- ▶ Model complexity increasing (well/facility models, fluid models)
- ▶ New mechanisms (polymer, CO₂) require better resolved fronts
- ▶ Large ensembles for history matching, optimization, uncertainty quantification

The market situation

Commercial reservoir simulators (expensive but comprehensive):

- ▶ ECLIPSE, Intersect (Schlumberger)
- ▶ IMEX, GEM, STARS (CMG)
- ▶ Nexus (Landmark)
- ▶ tNavigator (Rock Flow Dynamics)
- ▶ ...

In-house simulators (unavailable to outsiders):

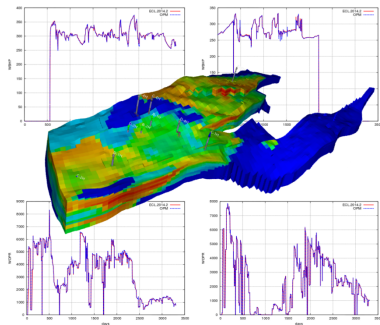
- ▶ (Tera)POWERS (Saudi-Aramco)
- ▶ MoReS (Shell)
- ▶ GPRS (Stanford University)
- ▶ ...

Open source simulators:

- ▶ OPM Flow
- ▶ MRST (Sintef)

OPM Flow at a glance

- ▶ Open source
- ▶ Handling cases of full industrial complexity (wells, properties)
- ▶ Competitive performance
- ▶ Currently used to study (for example):
 - ▶ Oil production: history matching and prediction of field performance
 - ▶ Enhanced oil recovery: CO₂, polymer
 - ▶ CO₂ sequestration
- ▶ Automatic differentiation enables rapid development of fluid models.



Ambition: to be a strong base for both industrial development and academic research

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What next?

- ▶ Conservation of mass
 - ▶ for each fluid pseudocomponent (oil, gas, water)
 - ▶ for injected EOR fluids (polymer, CO₂, surfactants)
 - ▶ (for ion species)
 - ▶ $\frac{\partial}{\partial t} (\phi A_\alpha) + \nabla \cdot \mathbf{u}_\alpha = Q_\alpha$

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- ▶ Multiphase flow: relative permeability and capillary pressure
 - ▶ flow rate reduced by k_r , function of fluid saturations
 - ▶ pressure difference between phases
 - ▶ $\mathbf{v}_\alpha = -(k_{r,\alpha}/\mu_\alpha)\mathbf{K}(\nabla p_\alpha - \rho_\alpha\mathbf{g})$

The black-oil model

- ▶ “Black-oil” model assumptions
 - ▶ Lump HC species into two (pseudo)components (oil, gas)
 - ▶ Allow oleic *phase* to contain both oil and gas *components*
 - ▶ Dissolved gas ratio, r_S
 - ▶ Allow gaseous *phase* to contain both oil and gas *components*
 - ▶ Vaporized oil ratio, r_V
 - ▶ Assumed always at thermodynamic equilibrium
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 - ▶ undersaturated oil (no gaseous phase)
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- ▶ (Subset of more general *compositional* model, must solve equation of state, such as Peng-Robinson)

System of equations

The continuous equations form a system of partial differential equations, one for each pseudo-component α :

$$\frac{\partial}{\partial t} (\phi A_\alpha) + \nabla \cdot \mathbf{u}_\alpha = Q_\alpha \quad (1)$$

where

$$A_w = m_\phi b_w s_w, \quad \mathbf{u}_w = b_w \mathbf{v}_w, \quad (2)$$

$$A_o = m_\phi (b_o s_o + r_V b_g s_g), \quad \mathbf{u}_o = b_o \mathbf{v}_o + r_V b_g \mathbf{v}_g, \quad (3)$$

$$A_g = m_\phi (b_g s_g + r_S b_o s_o), \quad \mathbf{u}_g = b_g \mathbf{v}_g + r_S b_o \mathbf{v}_o. \quad (4)$$

and these additional relations should hold:

$$s_w + s_o + s_g = 1 \quad (5)$$

$$p_{cow} = p_o - p_w \quad (6)$$

$$p_{cog} = p_o - p_g. \quad (7)$$

The phase fluxes are given by Darcy's law:

$$\mathbf{v}_\alpha = -\lambda_\alpha \mathbf{K} (\nabla p_\alpha - \rho_\alpha \mathbf{g}). \quad (8)$$

What is the source term, anyway?

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Well rates!

- ▶ Computed using separate well model(s).
- ▶ Must be solved *simultaneously* with reservoir equations.

Discretization

The system is discretized using:

- ▶ First-order implicit Euler in time
- ▶ First-order finite volumes in space
 - ▶ two-point flux approximation (!)
 - ▶ phase-based upwinding of properties

Why such “primitive methods” (low order, inconsistent)?

- ▶ Historically, finite difference methods
- ▶ Need systems that linear solvers can deal with well
- ▶ Sufficient for practical purposes
- ▶ Discretization errors not significant compared to inherent uncertainty

Quite a bit *has* been done by various groups (not mainstream yet):

- ▶ Consistent discretizations (MPFA, mimetic)
- ▶ Higher-order FV or DG methods
- ▶ Higher-order time discretizations

Discrete equations (I)

The discretized equations and residuals are, for each pseudo-component α and cell i :

$$R_{\alpha,i} = \frac{\phi_{0,i} V_i}{\Delta t} (A_{\alpha,i} - A_{\alpha,i}^0) + \sum_{j \in C(i)} u_{\alpha,ij} + Q_{\alpha,i} = 0 \quad (9)$$

where

$$A_w = m_\phi b_w s_w, \quad u_w = b_w v_w, \quad (10)$$

$$A_o = m_\phi (b_o s_o + r_{og} b_g s_g), \quad u_o = b_o v_o + r_{og} b_g v_g, \quad (11)$$

$$A_g = m_\phi (b_g s_g + r_{go} b_o s_o), \quad u_g = b_g v_g + r_{go} b_o v_o. \quad (12)$$

The relations (5), (6) and (7) hold for each cell i .

The fluxes are given for each connection ij by:

$$(b_\alpha v_\alpha)_{ij} = (b_\alpha \lambda_\alpha m_T)_{U(\alpha,ij)} T_{ij} \Delta H_{\alpha,ij} \quad (13)$$

$$(r_{\beta\alpha} b_\alpha v_\alpha)_{ij} = (r_{\beta\alpha} b_\alpha \lambda_\alpha m_T)_{U(\alpha,ij)} T_{ij} \Delta H_{\alpha,ij} \quad (14)$$

$$\Delta H_{\alpha,ij} = p_{\alpha,i} - p_{\alpha,j} - g \rho_{\alpha,ij} (z_i - z_j) \quad (15)$$

$$\rho_{\alpha,ij} = (\rho_{\alpha,i} + \rho_{\alpha,j})/2 \quad (16)$$

$$U(\alpha, ij) = \begin{cases} i & \Delta H_{\alpha,ij} \geq 0 \\ j & \Delta H_{\alpha,ij} < 0 \end{cases} \quad (17)$$

Solving the discrete equations

Main method: Newton-Raphson

- ▶ solve large heterogenous linear systems
- ▶ challenging to precondition (CPR + AMG best?)
- ▶ must modify updates for phase changes
- ▶ must handle convergence failures (timestep cuts)

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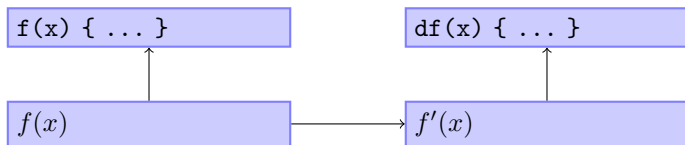
Implementation with automatic differentiation

What next?

What does AD provide

 $f(x) \{ \dots \}$ $df(x) \{ \dots \}$ $f(x)$ $f'(x)$

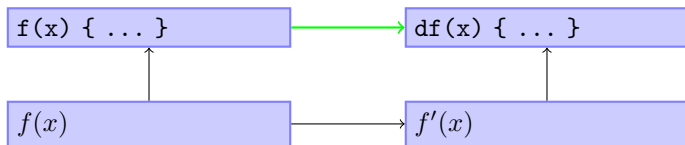
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Traditional Process

- ▶ Human implements code to evaluate $f(x)$
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Automatic Differentiation (AD)

- ▶ Human implements code to evaluate $f(x)$
- ▶ Computer code to evaluate $f'(x)$ is automatically generated

Benefits of using AD

AD makes it easier to create simulators:

- ▶ only specify nonlinear residual equation
- ▶ automatically evaluates Jacobian
- ▶ sparsity structure of Jacobian automatically generated

Note that AD is *not* the same as finite differencing!

- ▶ no need to define a 'small' epsilon
- ▶ as precise as hand-made Jacobian
- ▶ ... but much less work!

Performance (of equation assembly) will usually be somewhat slower than a *good* hand-made Jacobian implementation.

A numeric computation $y = f(x)$ can be written ($D = \text{derivative}$)

$$y_1 = f_1(x) \quad \frac{dy_1}{dx}(x) = Df_1(x)$$

$$y_2 = f_2(y_1) \quad \frac{dy_2}{dx}(x) = Df_2(y_1) \cdot Df_1(x)$$

\vdots

$$y = f_n(y_{n-1}) \quad \frac{dy}{dx}(x) = Df_n(y_{n-1}) \cdot Df_{n-1}(y_{n-2}) \cdots Df_1(x)$$

Automatic Differentiation:

- ▶ make each line an elementary operation
- ▶ compute right derivative values as we go using chain rule

Implementation approaches

Two main methods:

Operator overloading

- ▶ requires operator overloading in programming language
- ▶ syntax (more or less) like before (non-AD)
- ▶ efficiency can vary a lot, depends on usage scenario
- ▶ easy to implement and experiment with
- ▶ Examples: OPM, Sacado (Trilinos), ADOL-C

Source transformation with AD tool

- ▶ can be implemented for almost any language
- ▶ may restrict language syntax or features used
- ▶ efficiency can be high (depends on AD tool)
- ▶ Examples: TAPENADE, OpenAD

Types of AD

Two different approaches.

(We compute $f(x)$, u is some intermediate variable.)

Forward Mode

Carry derivatives with respect to independent variables:

$$(u, \frac{du}{dx})$$

Reverse Mode

Carry derivatives with respect to dependent variables (adjoints):

$$(u, \frac{df}{du})$$

Forward AD example (1)

Example function: $f(x) = x(\sin(x^2) + 3x)$.

Sequence of elementary functions:

$$f_1(u) = u^2$$

$$f_2(u) = \sin(u)$$

$$f_3(u) = 3u$$

$$f_4(u, v) = u + v$$

$$f_5(u, v) = u \cdot v$$

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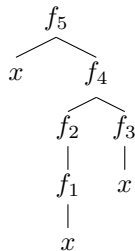
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Rewritten:

$$f(x) = f_5(x, f_4(f_2(f_1(x)), f_3(x)))$$



Forward AD example (2)

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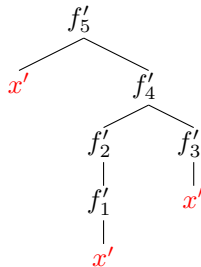
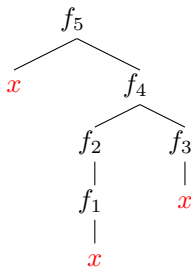
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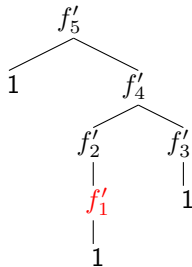
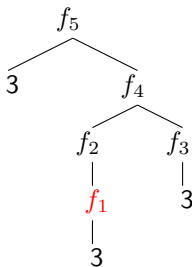
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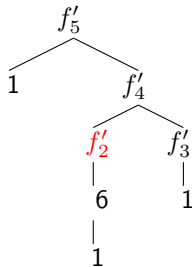
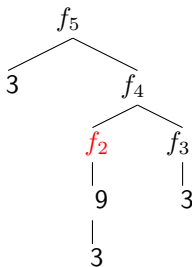
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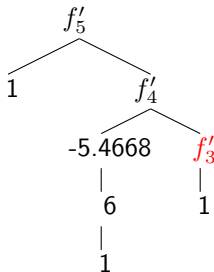
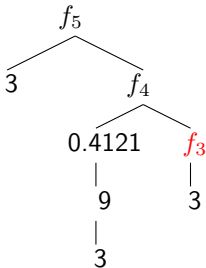
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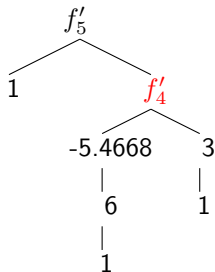
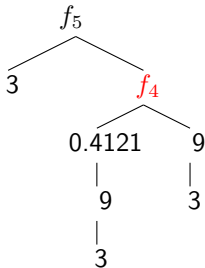
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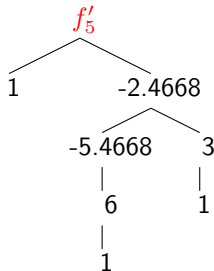
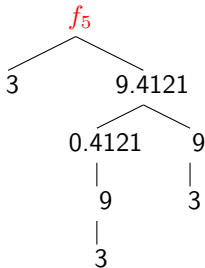
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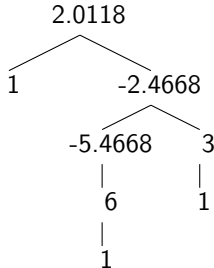
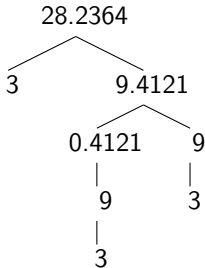
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- ▶ Easy to implement with operator overloading
- ▶ Storage required (scalar): $2 \times$ normal (value, derivative).
- ▶ Storage required ($f : R^m \rightarrow R^n$): $(n + 1) \times$ normal (value, derivative vector), unless sparse.

Recall: Reverse Mode

Carry derivatives with respect to dependent variables (adjoints):

$$(u, \frac{df}{du})$$

We will use the chain rule again, but in the opposite direction:

$$\text{adj}(u) = \text{adj}(f_i) \frac{\partial f_i}{\partial u}.$$

Using $\text{adj}(u)$ to mean the adjoint $\frac{df}{du}$.
(So $\text{adj}(x)$ is our goal.)

Reverse AD example

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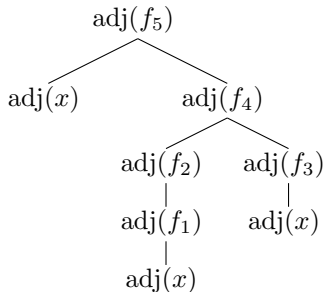
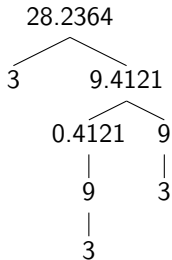
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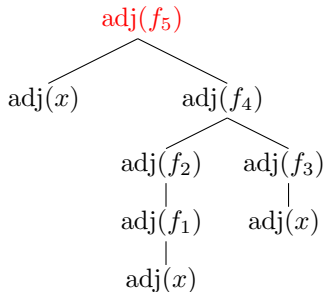
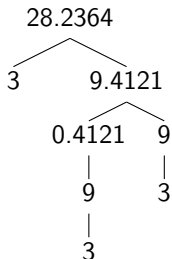
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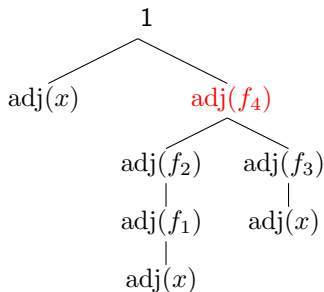
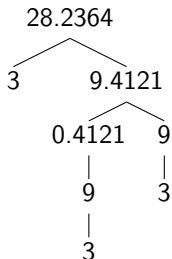
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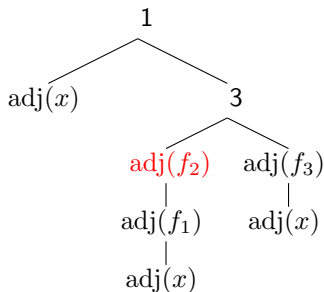
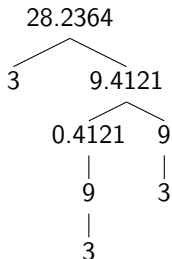
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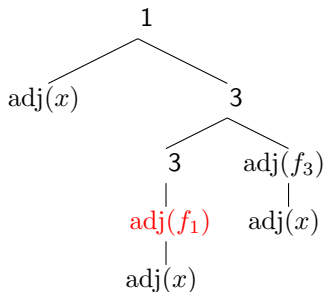
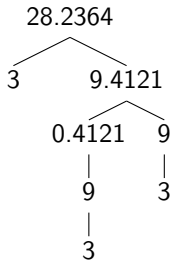
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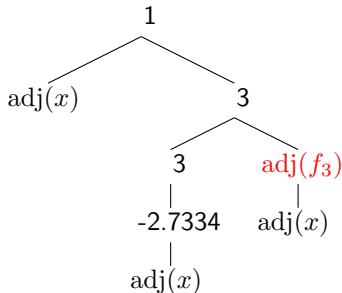
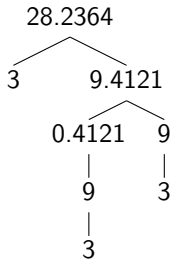
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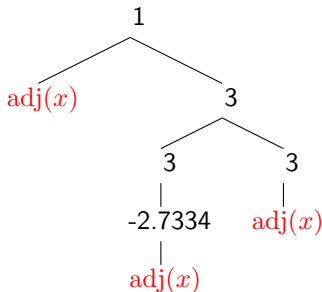
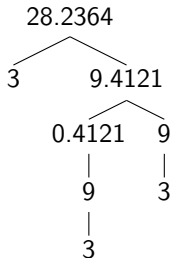
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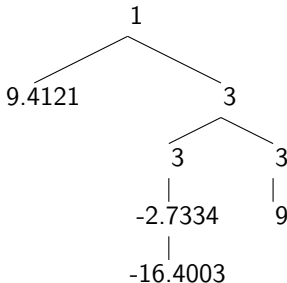
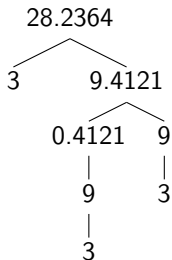
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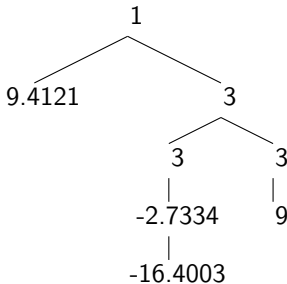
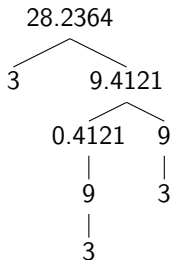
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Must sum
contributions:
 $f'(3) = 9.4121 -$
 $16.4003 + 9 = 2.0118.$

Automatic Differentiation: OPM implementations

AutoDiffBlock (legacy)

- ▶ class implementing *forward AD*
- ▶ deals with *vectors of values* at a time
- ▶ derivatives are *sparse matrices*
- ▶ implemented with operator overloading
- ▶ based on Eigen library for basic types and operands
- ▶ helper library provides discrete div, grad etc.

Evaluation (new effort)

- ▶ class implementing *forward AD*
- ▶ deals with *a single scalar value* at a time
- ▶ derivatives are *compile-time-size vectors*
- ▶ implemented with operator overloading
- ▶ discrete div, grad must be implemented “manually”

Overview of talk

Reservoir simulation

Mathematical formulation

Implementation with automatic differentiation

What next?

We keep pursuing...

- ▶ Performance
 - ▶ Improving preconditioners and linear solvers
 - ▶ New discretizations, nonlinear preconditioning
 - ▶ Parallel scaling
- ▶ Usability
 - ▶ Reference manual started!
 - ▶ More output/logging options
 - ▶ Better error messages
- ▶ Deployability
 - ▶ Container usage
 - ▶ MSO4SC Portal and web integration
 - ▶ Better error messages

Further ahead: some possibilities

- ▶ New fluid models for CO₂, EOR options.
- ▶ Scriptable? Python? Cling-able?
- ▶ More flexible boundary conditions
- ▶ Higher order DG methods?
- ▶ Consistent discretizations?
- ▶ Fully compositional fluid model?
- ▶ New I/O system for parallel scalability?
- ▶ Preprocessing tools?

Thank you for listening!

