

Compositional Simulation with OPM-flow

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Contributors



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A small history



- PT-Flash calculation June 2022
- A pressure driven CO₂ flooding 1D demonstration Nov. 2023
- Extending fluid system to allow any number of components
 - Oil-Gas two phase Dec. 2023
- Running simulation from DATA input file Sep. 2024
- Summary and Restart output Oct. 2024
- Compositional well modeling -> ongoing

Compositional reservoir simulation



- Mass balance equations for N components

$$\frac{\mathbf{M}_i^{n+1} - \mathbf{M}_i^n}{\Delta t^n} + \operatorname{div}(\mathbf{V}_i) - \mathbf{Q}_i = 0, \quad i \in \{1, \dots, N\}.$$

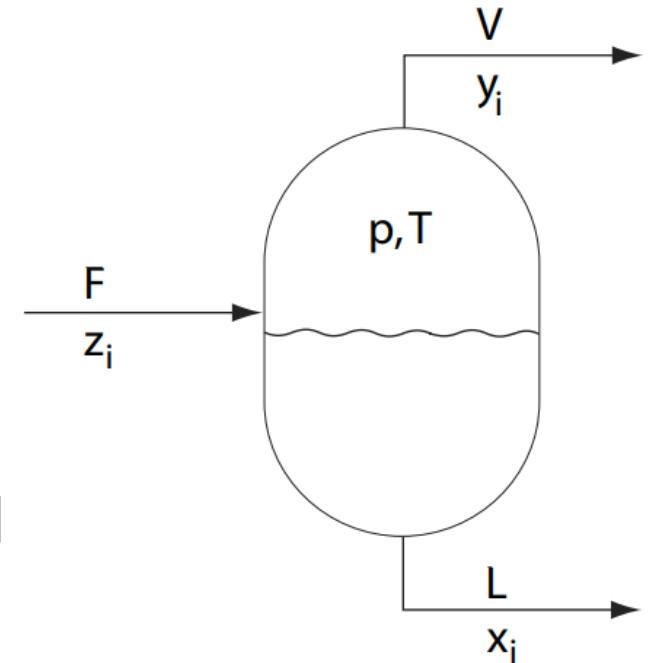
$$\mathbf{M}_i = \Phi(\rho_\ell S_\ell X_i + \rho_v S_v Y_i)$$

$$\mathbf{V}_i = -\mathbf{T}^f (\lambda_{i,\ell}^f \Theta_\ell + \lambda_{i,v}^f \Theta_v)$$

$$\sum_i^N x_i = 1, \quad \sum_i^N y_i = 1, \quad S_\ell + S_v = 1, \quad p_v = p_\ell + p_{cv\ell}$$

Isothermal flash calculation

- Vapor Liquid two phase
 - fugacity equilibrium
- Peng-Robinson equation of states
- Stability test
- Successive substitution iteration (SSI), Newton method and Hybrid SSI-Newton
- Automatic differentiation (AD)



Supported compositional keywords



- COMPS
- EOS
- CNAMES
- ACF, MW, PCRIT, TCRIT, VCRIT, BIC

- XMF, YMF, ZMF

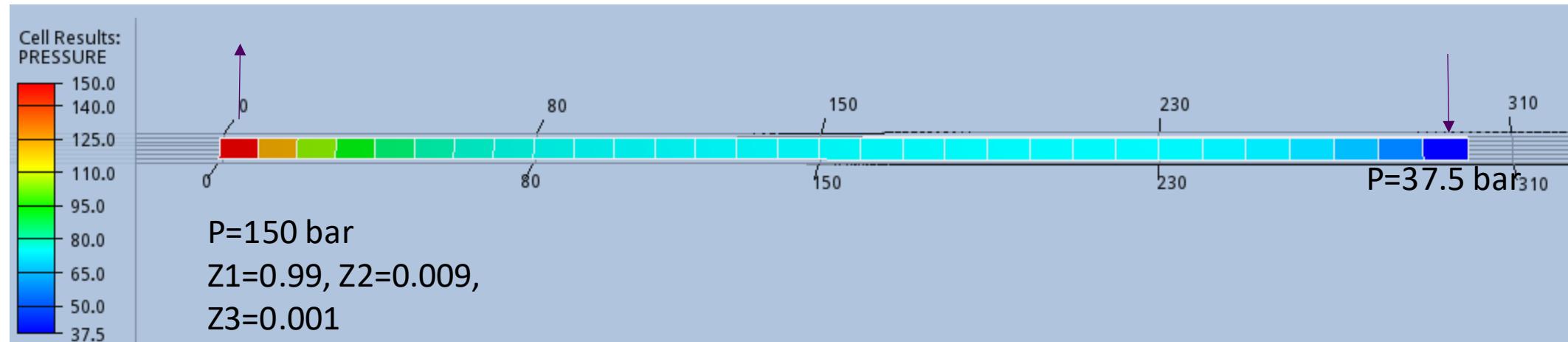
Demonstration



- `flowexp_comp`
- arguments:
 - `--ecl-deck-file-name` (input file)
 - `--output-dir` (output path)
 - `--enable-vtk-output` (false by default)
 - `--flash-two-phase-method` (ssi, newton and ssi+newton, ssi by default)
 - `--flash-verbosity` (0 by default)
- `flowexp_comp --ecl-deck-file-name=SIMPLE_COMP_SMALLZ.DATA`
`--output-dir=outputdir --enable-vtk-output=true`

Test Case

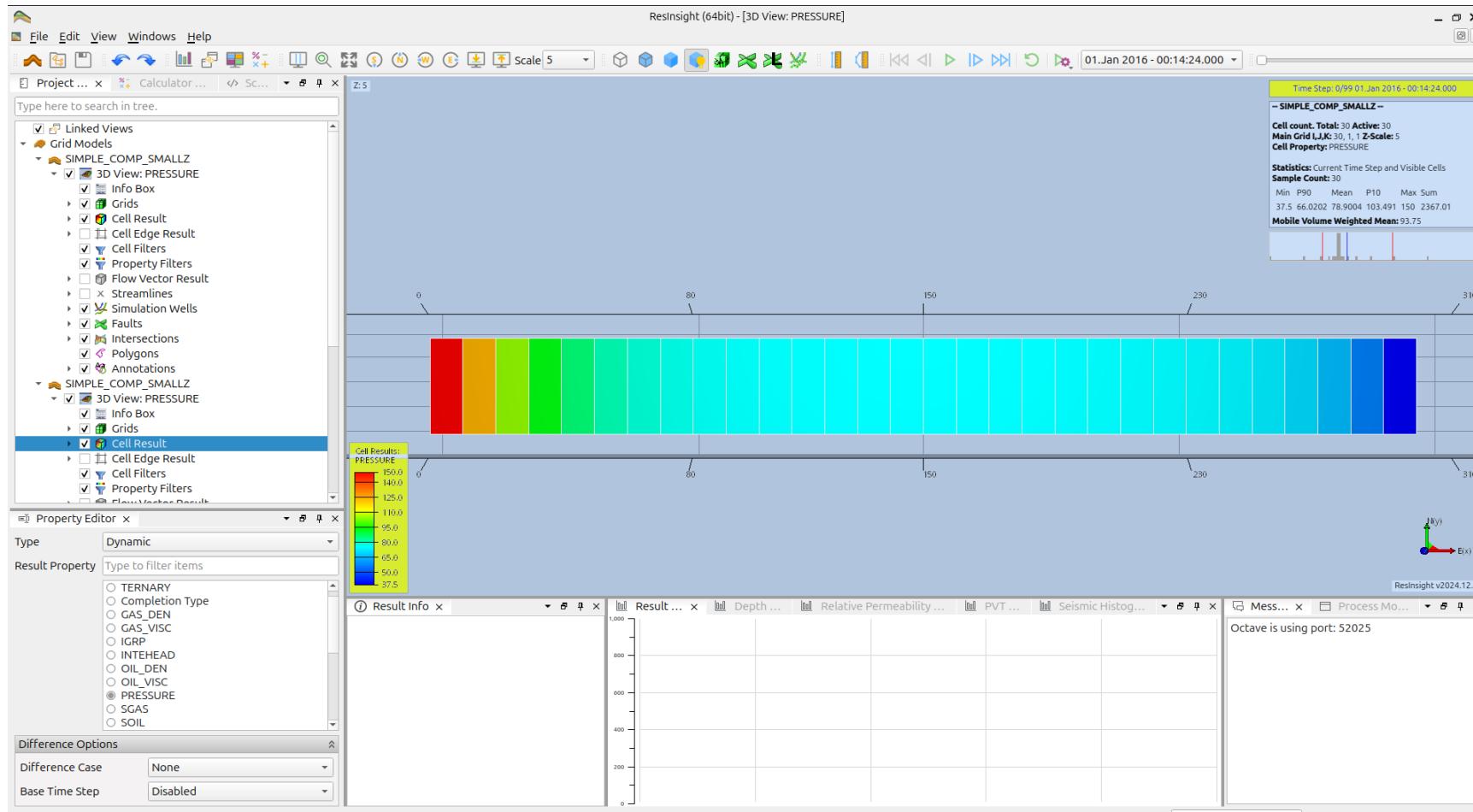
- 1-D model (30x1x1)
- $K=100 \text{ mD}$, $\Phi=0.1$, $P_{\text{res}}=75 \text{ bar}$, $S_{\text{Gas}}=1$, $T_{\text{res}}=150 \text{ }^{\circ}\text{C}$,
- Components (CO₂(1), CH₄(2), Decane(3)), $Z_1=0.5$, $Z_2=0.3$, $Z_3=0.2$
- Cell(1,1,1) and cell(30,1,1) are assigned with much bigger pore volume to mimic source and sink with constant pressure and compositions



Visualization



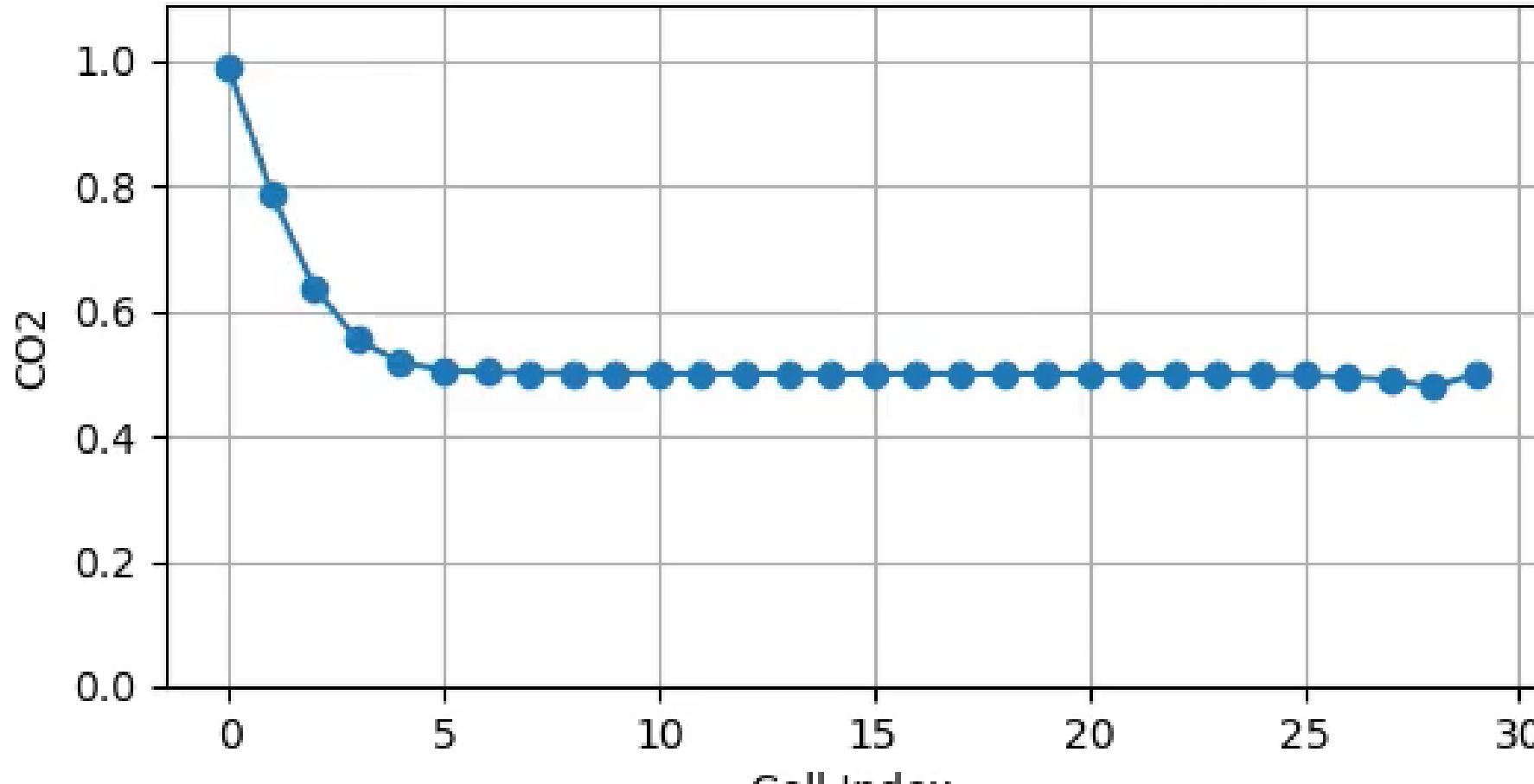
- ResInsight and Paraview can be used to visualize the output



Resulting CO₂ mole fraction evolution



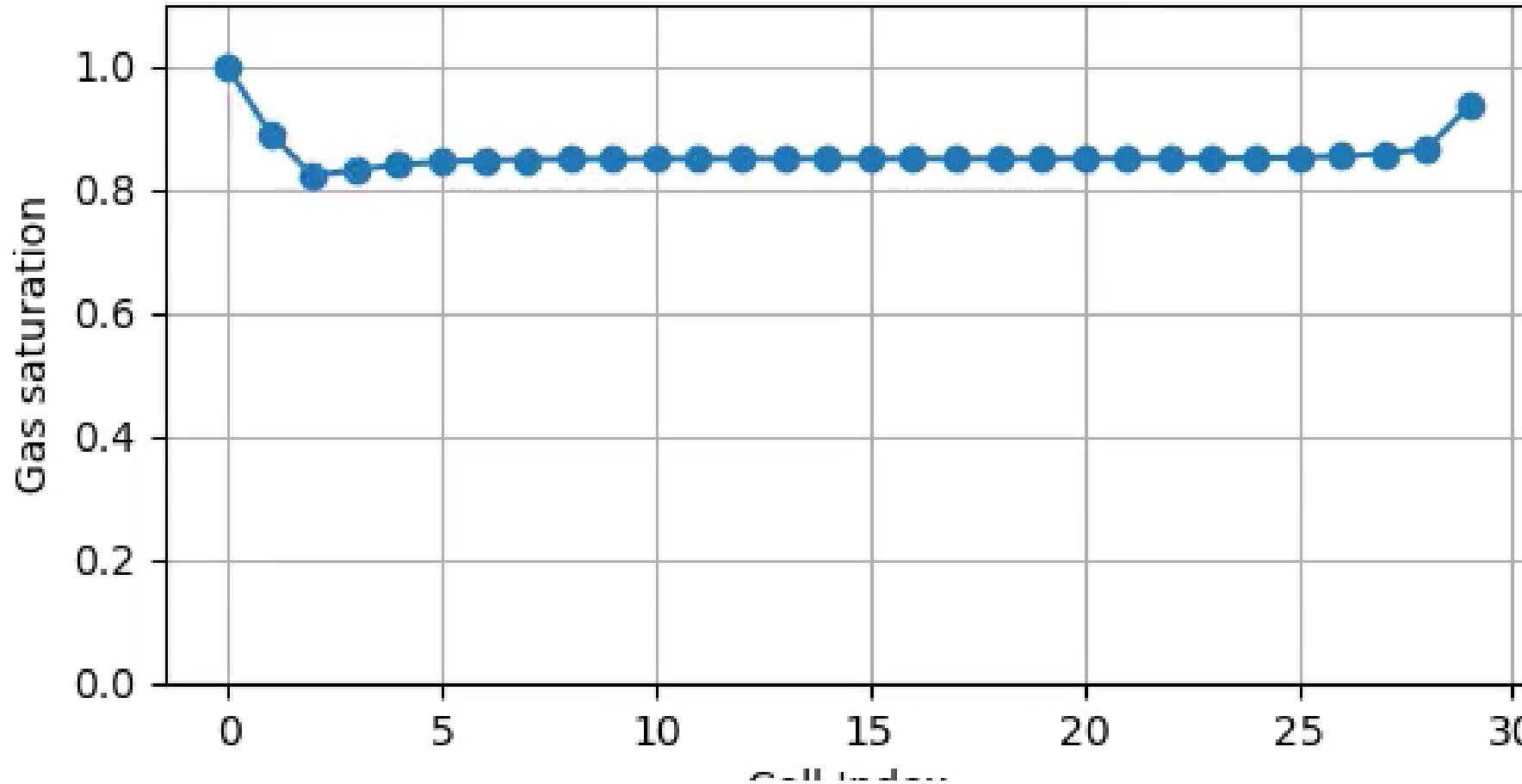
CO₂ mole fraction at Time Step 1



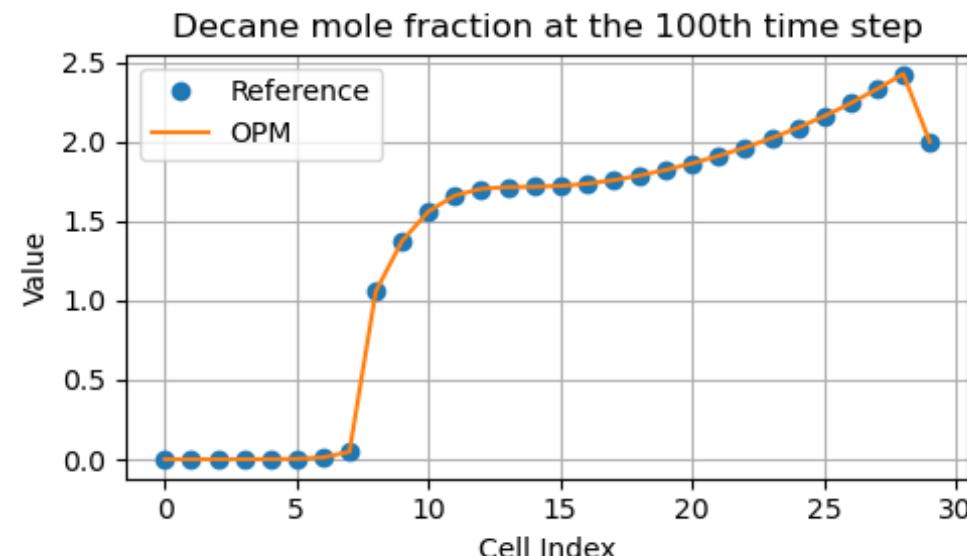
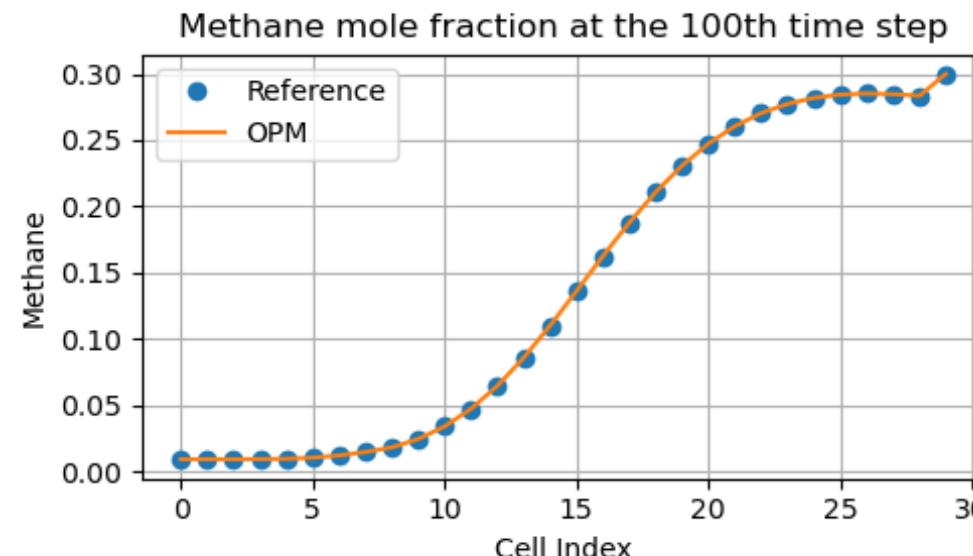
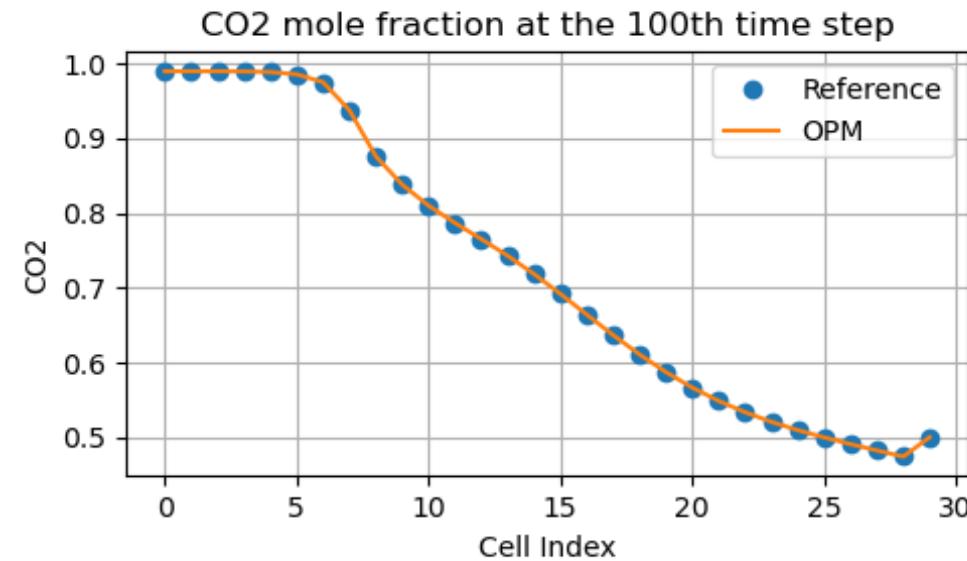
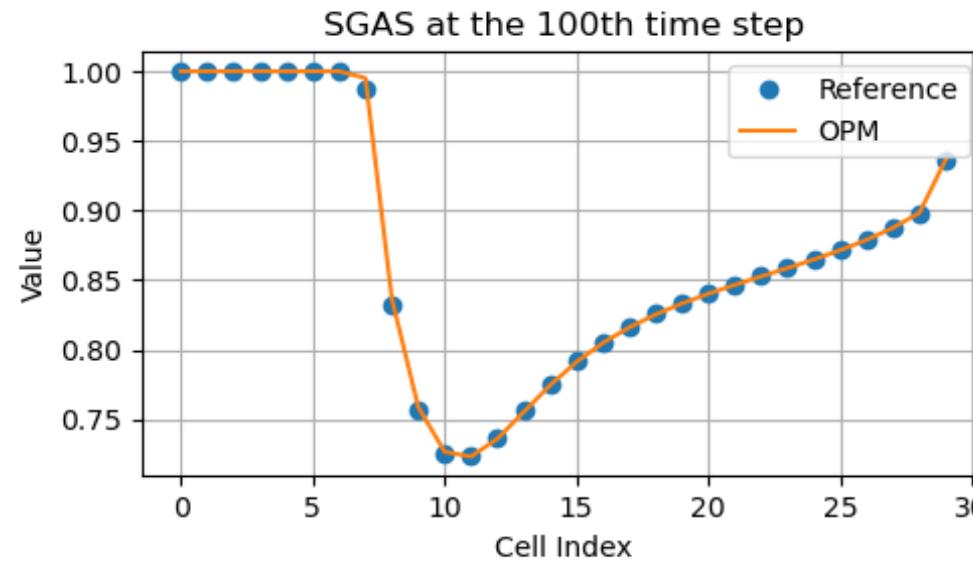
Resulting gas saturation evolution



Gas saturation at Time Step 1



Validation against reference result



Features expected for OPM Release 25.04



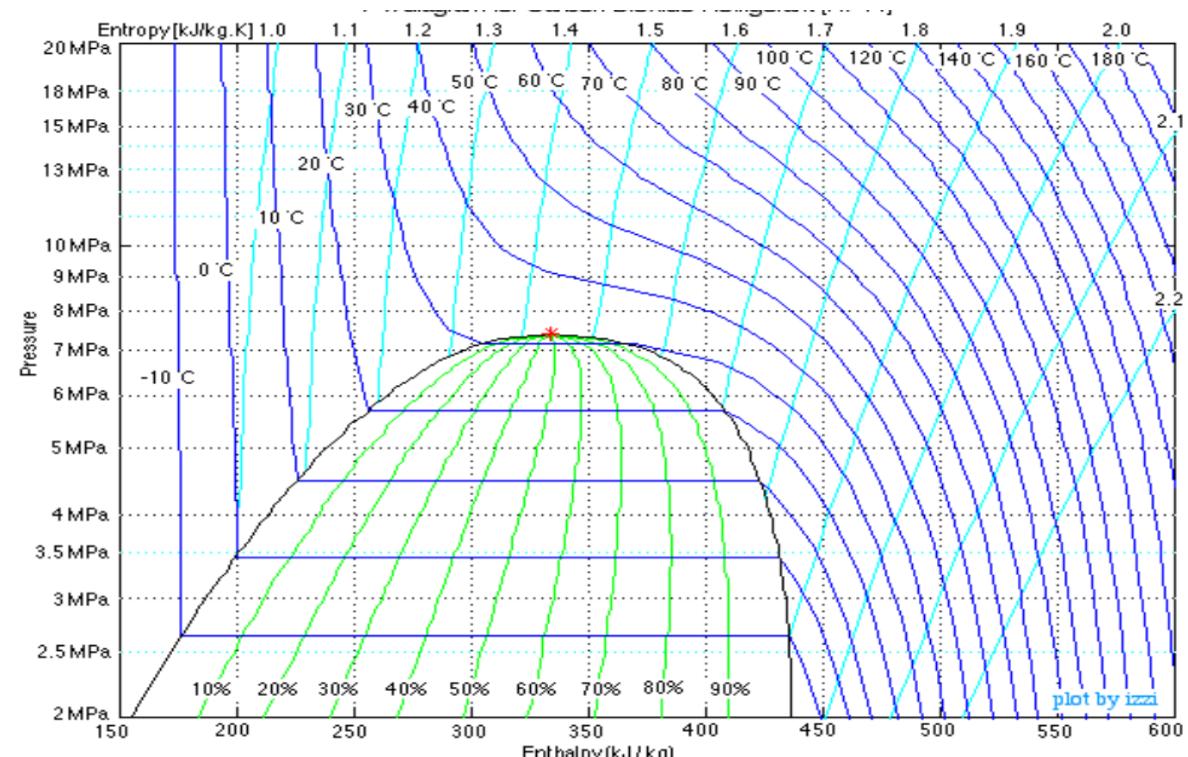
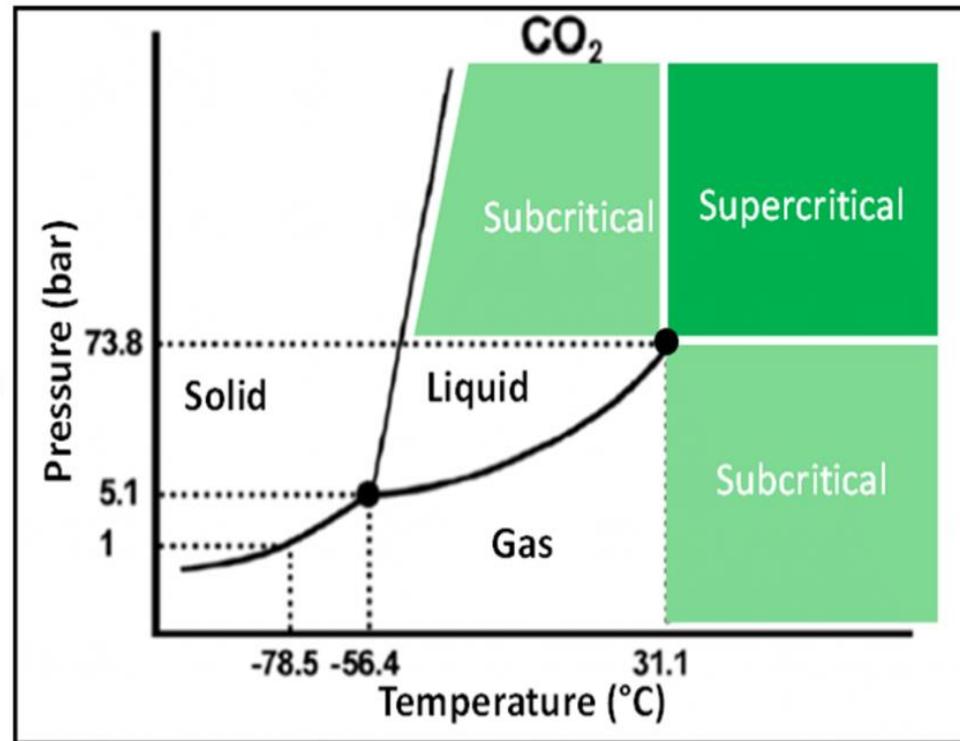
- Compositional Standard Well model (working in process)
- Three phase with water
 - water is not involved in flash calculation
- Equilibration initialization

Hopefully

- Testing with bigger models for CO₂ injection
- Thermal

EOS Based Thermal Compositional Energy Balance Formulation - Enthalpy Formulation

$$\frac{\partial}{\partial t} \left[\phi \left(\sum_{j=1}^{np} \rho_j S_j U_j \right) + (1-\phi) \rho_r U_r \right] = -\nabla \cdot \left(\sum_{j=1}^{np} \rho_j h_j u_j \right) + \nabla \cdot (K_T \nabla T) + q_H$$



Summary



- It is still in the early stage.
 - Testing, refactoring, optimization, adding features
- It can be readily elevated by incorporating existing capacities from flow simulator
 - Parsing, schedule, grid, parallelization, linear solvers, input/output facility, etc.
- It is on the way to be ready for future research and application.

Thank you!